The large-scale capture and sequestration of carbon dioxide (CO\textsubscript{2}) from pre-combustion, post-combustion, and natural gas mixtures have become important technological and environmental targets to mitigate the effect of greenhouse gases on global climate change. Conventional CO\textsubscript{2} capture using primary alkanolamine scrubbers consumes large amounts of energy for regeneration. Nanoporous materials such as carbon molecular sieves, zeolites, and MOFs have been studied for CO\textsubscript{2} separations and capture because of their high internal surface area, high micropore volume, chemical tunability, fast adsorption/desorption kinetics, and low heats of adsorption [1].

Chabazite (CHA) is a small pore zeolite consisting of a double 6-membered ring (D6R) as the basic building unit with one large ellipsoidal cavity accessed by six 8-membered ring windows (8MR). CHA-type zeolites provide improved hydrothermal stability over other zeolites, an important property in the selective catalytic reduction of NO\textsubscript{x} and moist flue-gas applications. CHA has also been shown to have high selectivity for light olefins in the conversion of methanol to olefins process and demonstrated potential in gas separations, such as CO\textsubscript{2} from N\textsubscript{2} in flue gas mixtures. Extra-framework cations present in Al-exchanged zeolite frameworks play important roles in determining the adsorption properties.

Adsorption measurements reveal that the CHA samples with higher aluminum content have higher adsorption capacity. We considered the adsorption properties and site-specific adsorption properties of CO\textsubscript{2} in pure, high, and medium silica CHAs (Si/Al = ∞, = 12, = 6, respectively) with varied cation-exchange (Li\textsuperscript{+}, K\textsuperscript{+}, Na\textsuperscript{+}). These insights were obtained by combining in-situ X-ray (XRPD) and neutron powder diffraction (NPD) methods using Fourier difference mapping to locate the adsorbed CO\textsubscript{2} and correlating the results with adsorption measurements. This allows us to elucidate the atomic origin of the adsorption properties across a series of cation-exchanged zeolites, which aids in the engineering of improved CO\textsubscript{2} adsorbents [2].

Figure 1 depicts the locations of alkali metal cations typically observed in high-silica CHAs. From Rietveld refinement of powder diffraction data, we observed Li and Na at the 6MR window, as expected as this coordination environment is the most favorable in CHA for small cations. In this position, each Li\textsuperscript{+} or Na\textsuperscript{+} is effectively coordinated with 3 oxygen atoms of the framework. Due to ionic radii difference (r\textsubscript{Na\textsuperscript{+}} = 1.16 Å, r\textsubscript{Li\textsuperscript{+}} = 0.73 Å), Na\textsuperscript{+} lies higher above the plane of the 6MR (≈ 22°) measured from the Si in the ring compared to Li-CHA-6 (≈ 9.6°). These angles are slightly larger in Li- and Na-CHA-12. On the other hand, the larger K\textsuperscript{+} cation sits preferentially in the middle of the 8MR where it is coordinated with 4 oxygen atoms of the zeolite framework. In addition, K\textsuperscript{+} is observed on a position above the 6MR where it is only coordinated with 3 oxygen atoms of the zeolite framework.
CO₂ molecule to the surrounding oxygen atoms of the framework. The refinement of XRPD and NPD patterns of CO₂ on pure silica CHA resulted in the identification of two adsorption sites for CO₂: (1) locating in the 8MR and (2) in the ellipsoidal cages of CHA framework (Fig. 1). In the CHA 8MR, the preferred adsorption site (A) is the center of the CHA window in which each carbon atom in CO₂ molecule has maximal close contacts with the 8 oxygen atoms of the 8MR such that two O₈MR across the ring from each other give an angle O₈MR−C=O−O₈MR = 180°. From XRPD refinement of CO₂ in Si-CHA, the CO₂ – 8MR oxygen atom distances were determined to be from 3.129(6) Å to 3.410(4) Å, and with d(O⁺CO₂–O⁻CHA) between ca. 3.18 Å to 3.98 Å. Another CO₂ adsorption site (B) in pure silica CHA is inside the ellipsoidal cage where the carbon atom has the most effective contact distances with 4 framework oxygen atoms and the CO₂ oxygen atoms also have effective contact distances with 4 to 5 framework oxygen atoms each. Overall, these considerations explain the high occupancy of CO₂ at site A in CHA zeolites, or indeed in 8MR zeolites in general.

Two CO₂ adsorption sites were determined in Li-CHA and Na-CHA zeolites by Fourier analysis (Fig. 2). The distance between Na⁺ and CO₂ in site A (3.605(0) Å) is much shorter than that for the Li⁺ (4.307(0) Å) leading to a more effective electrostatic interaction. The CO₂ second site in these zeolites is end-on coordination with the cation, M⁺−O=C=O, at distances of 2.68(7) Å (Na⁺) and 2.3(2) Å (Li⁺). The linear CO₂ molecule is tilted toward the 4MR window to achieve closer contact with framework oxygen atoms. This adsorption site can be viewed as B' being a rotation and translation of the all-silica site (B). Since the Li⁺−O=C=O distance is shorter than that in Na⁺-CHA, the CO₂ contact angle is more acute, ∠Li⁺−O=C=O = 144° vs. ∠Na⁺−O=C=O = 163°, having more effective dispersive interaction with the framework. Because the interaction energy of the large quadrupole moment of CO₂ (14.3 × 10⁻⁴⁰ C m²) with an inhomogeneous electric field of zeolite is highest in 8MR zeolites, site A (8MR) is still a major adsorption site in alkali-exchanged CHA even though open metal cations provide an additional strong binding site in the cage (B') through enhanced electrostatic interaction.

In solid CO₂, molecules of CO₂ are arranged in their lowest energy configuration where an O atom of one CO₂ molecule is in close contact with more than 10 oxygen atoms and C atom also has close contact with 6 oxygen atoms of other CO₂ (dC−O = 3.11 Å), which is the distance we found in the 8MR. Further, in the cases of Li- and Na-CHA-12 at low CO₂ doses, there is an overall similarity of the positions and occupancies of the two CO₂ sites (A, B') with ∠Li⁺−O=C=O ≈ 142° and ∠Na⁺−O=C=O ≈ 166° and the cation-CO₂ distance are identical to those in CHA-6 at 2.302(5) Å (Li⁺) and 2.59(8) Å (Na⁺).

Refinement of the K-CHA-12 data show that K⁺ behaves quite similarly to Cu²⁺ in which the majority of the CO₂ is found in the 8MR and only a small fraction of the adsorbate is found with an end-on CO₂ coordination with the cations.Interestingly, in K-CHA-6 with the higher concentration of K⁺ partially blocking more of the 8MR window, the occupancy of the second CO₂ site (C) in the cage is significantly increased. The increase in interaction energy is due to the CO₂ coordination to two K⁺ cations (across 6MR-6MR or 6MR-8MR) being more efficient in lower silica K-CHA-6 with a K⁺−O=C=O distance approx. 3 Å. In this configuration, the oxygen and carbon atoms also have a number of attractive interactions with framework oxygen atoms.

Structural properties of Chabazite zeolites dosed with CO₂ were determined from in-situ powder X-ray and neutron diffraction measurements. The 8MR (A) was identified as the major CO₂ adsorption site in pure silica CHA due to the high number of close contacts to the framework oxygen atoms to the CO₂. The exchanged cations in charged CHA frameworks are open metal ions providing strong binding sites through induced polarizability of CO₂. CO₂ is coordinated end-on to cations with the molecular axis tilted to the framework to maximize its dispersion interaction. The population of the direct coordinated adsorption sites of CO₂ with these metal cations decreases with the hardness of cation, except for K-CHA-6, where the bridged complexes of CO₂ and two K⁺ cation sites were formed with higher interaction energy than a single cation adsorption site. Additionally, a major CO₂ adsorption site in the 8MR, previously determined in Cu-CHA [3], was still observed in these cation-exchanged CHAs due to high van der Waals and quadrupole interactions. The type of structural determination completed here is essential in the understanding and design of better absorbent materials for CO₂ capture and separation technologies.

**References**

